

# Improving Energy Efficiency and Effluent Quality and Reducing Operating Costs by Controlling Nitrification and Denitrification Through Operational Modifications



Presented by:  
**Joseph R. Tamburini**

- Rockaway Valley Regional Sewerage Authority
  - Edward Ho, P.E.
  - Robert Sobeck, P.E.
- Rothberg, Tamburini & Winsor, Inc.
  - Ronald G. Schuyler

# Purpose



- Good Effluent Quality
  - Improve effluent quality while saving money
- Minimize Construction Costs
  - No additional construction required
- Save Money
  - Power savings
  - Chemical savings
  - Increased energy efficiency

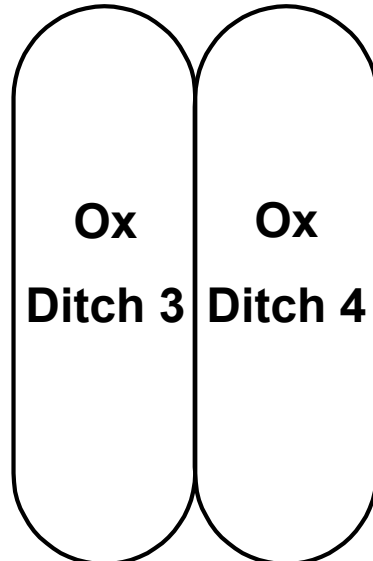
- Introduction
- Good Effluent Quality
- Review Issues Facing RVRSA
  - Stringent permit limits
  - Increasing flow and BOD loading
- Solution: Operational Process Control
  - Resolve issues facing plant
- Cost and Energy Savings
- Other Benefits

# Introduction: General

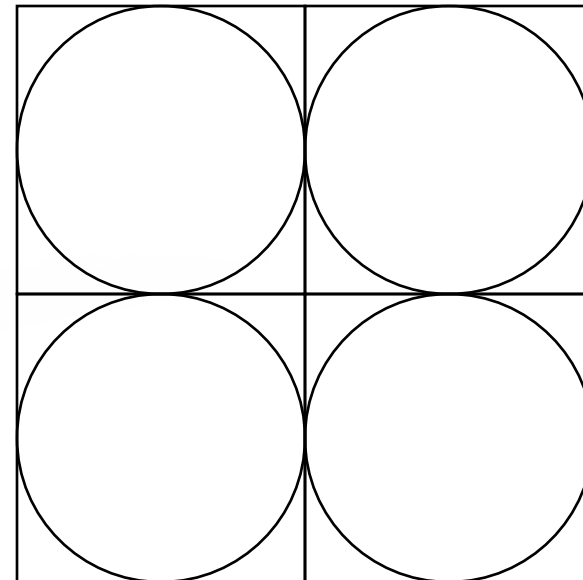
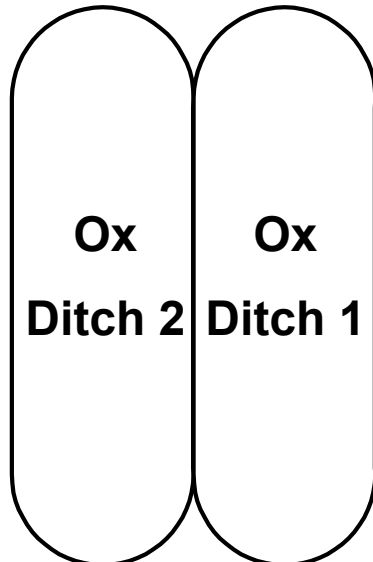


- Rockaway Valley Regional Sewerage Authority
- Configuration
  - Extended air, oxidation ditches
- Aeration: Rotating brush – no VFDs
- Discharge: Passaic River
- Contacts
  - Executive Director: Edward Ho, P.E.
  - Operations Supervisor: Robert Sobeck, P.E.

# Introduction: Plant Schematic



**Oxidation Ditches**



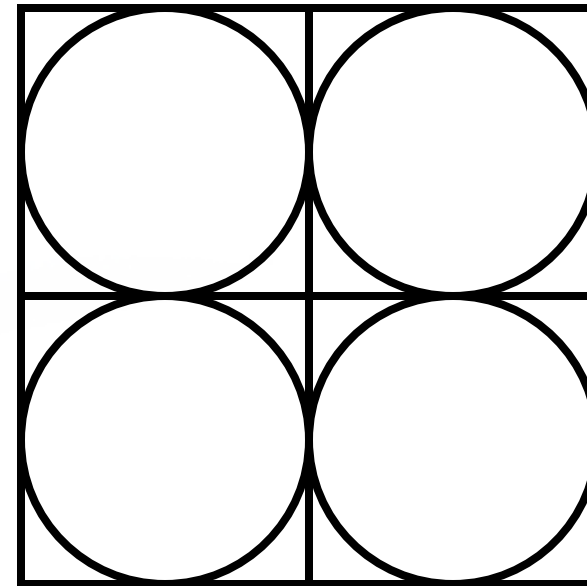
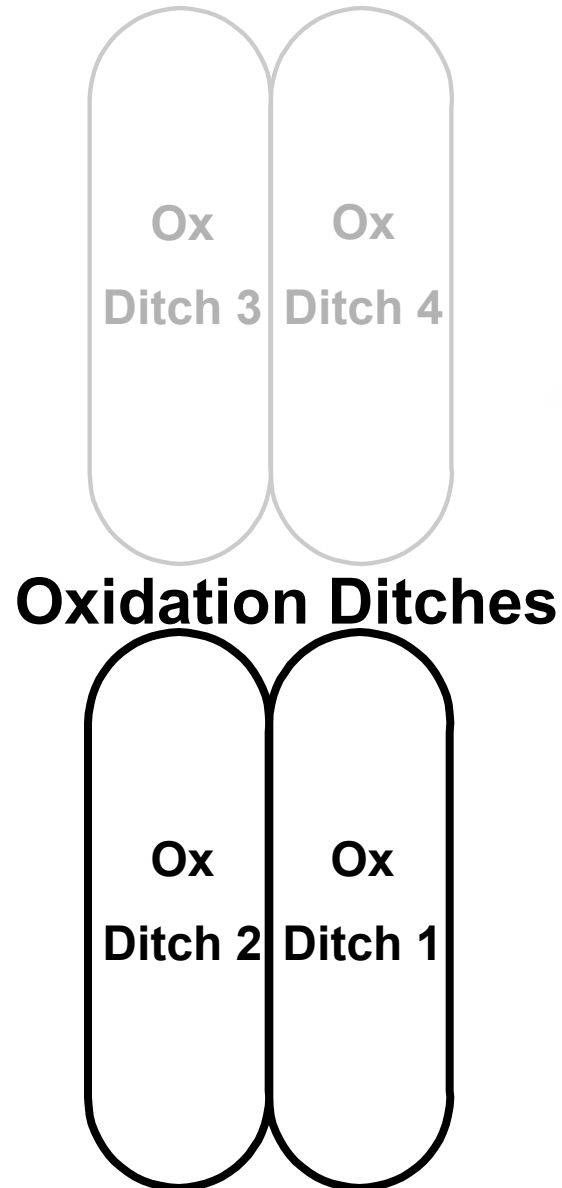
**Final Clarifiers**

# Introduction: Initial Design Criteria



- Original Rated Capacity: 12.0 MGD
- Design Loadings
  - HRT: 22 hrs
  - Organic Loading: 15.1 lbs cBOD/1000ft<sup>3</sup>/d
  - Clarifiers: 382 gal/ft<sup>2</sup>/d
- Original Operating Parameters
  - MCRT: 10+ days
  - MLSS: <2,000 mg/L

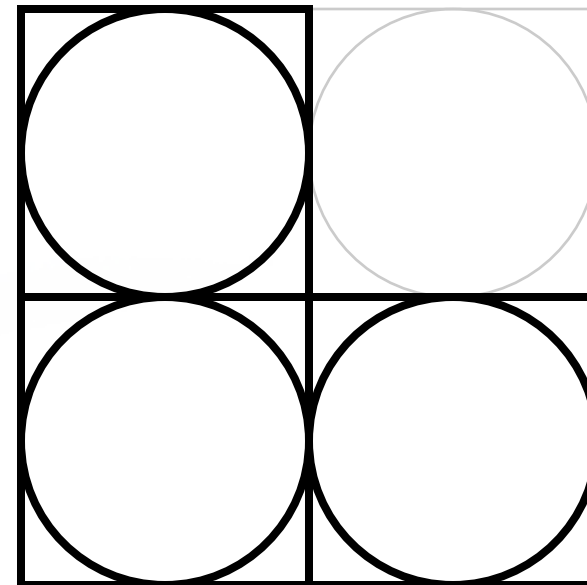
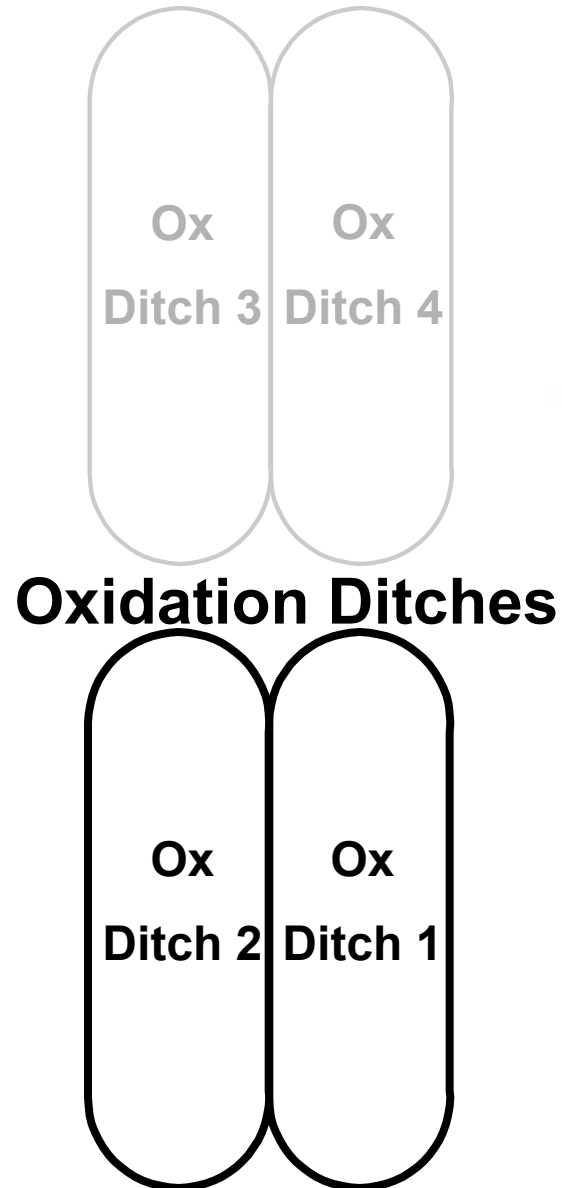
# Introduction: Current Operation



**Final Clarifiers**

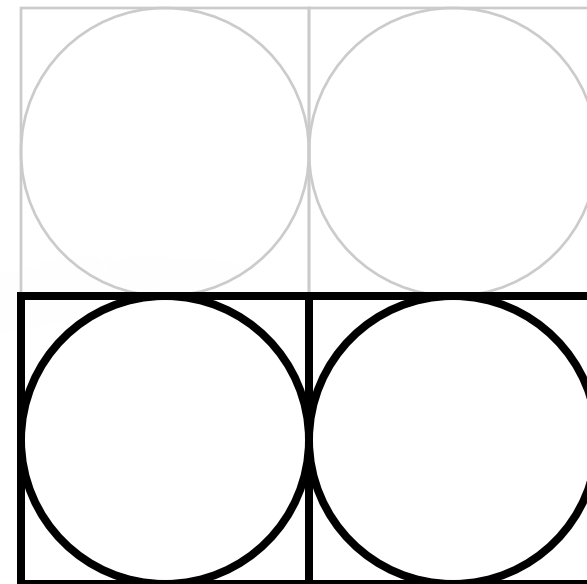
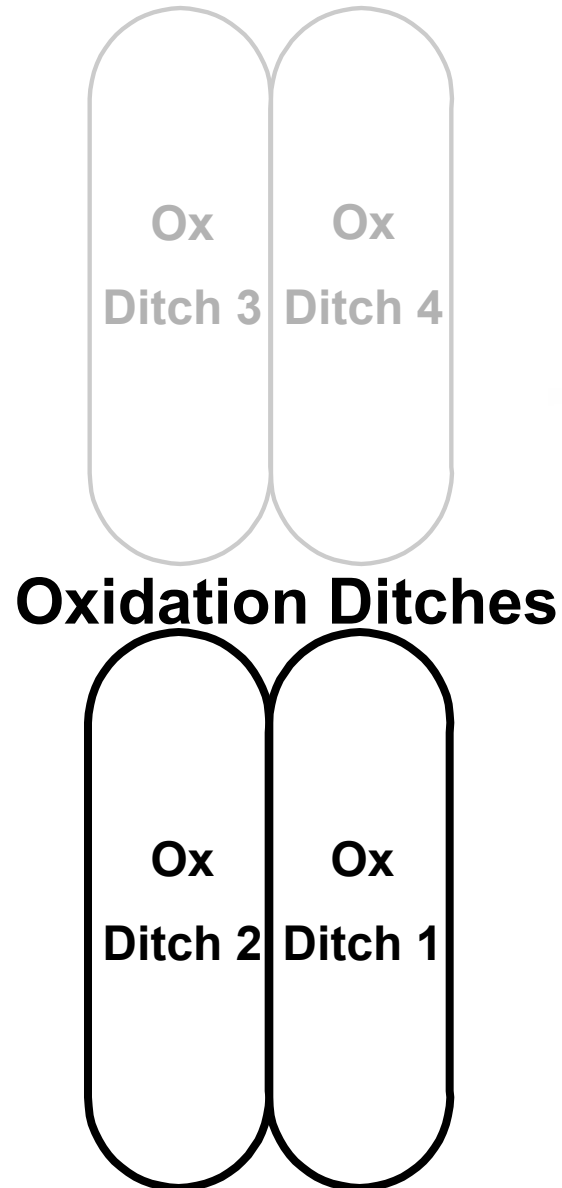


# Introduction: Current Operation

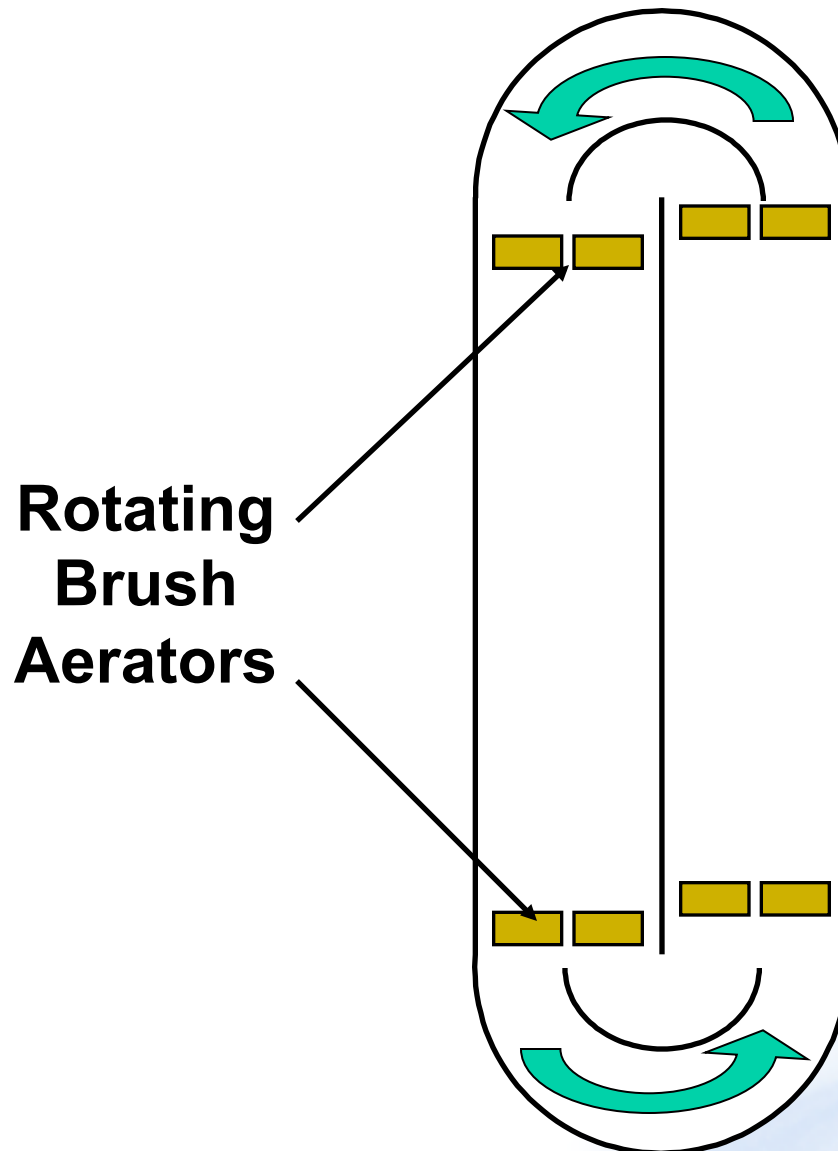


Final Clarifiers

# Introduction: Current Operation



# Introduction: Oxidation Ditches



**4 Aerators per ditch**

**- 100 hp per aerator**

# Good Effluent Quality: What is it?



- What is good effluent?
  - Meets permit limits?
  - Exceeds permit limits
  - Also: **Economical**
- What is necessary to make good effluent?
  - Capable plant
  - Proper process control

# Good Effluent Quality: Permit Limits



- Permit Effluent Limits (monthly average)
  - cBOD: 8 mg/L
  - TSS: 30 mg/L
  - NH<sub>3</sub>-N: May-Oct 1.8 mg/L  
Nov-Apr 6.0 mg/L
  - TMDLs recently established for Total Phosphorus
    - Possible future TP limit ~0.8 mg/L
- Currently No Total Nitrogen Limit

# Issues Facing RVRSA



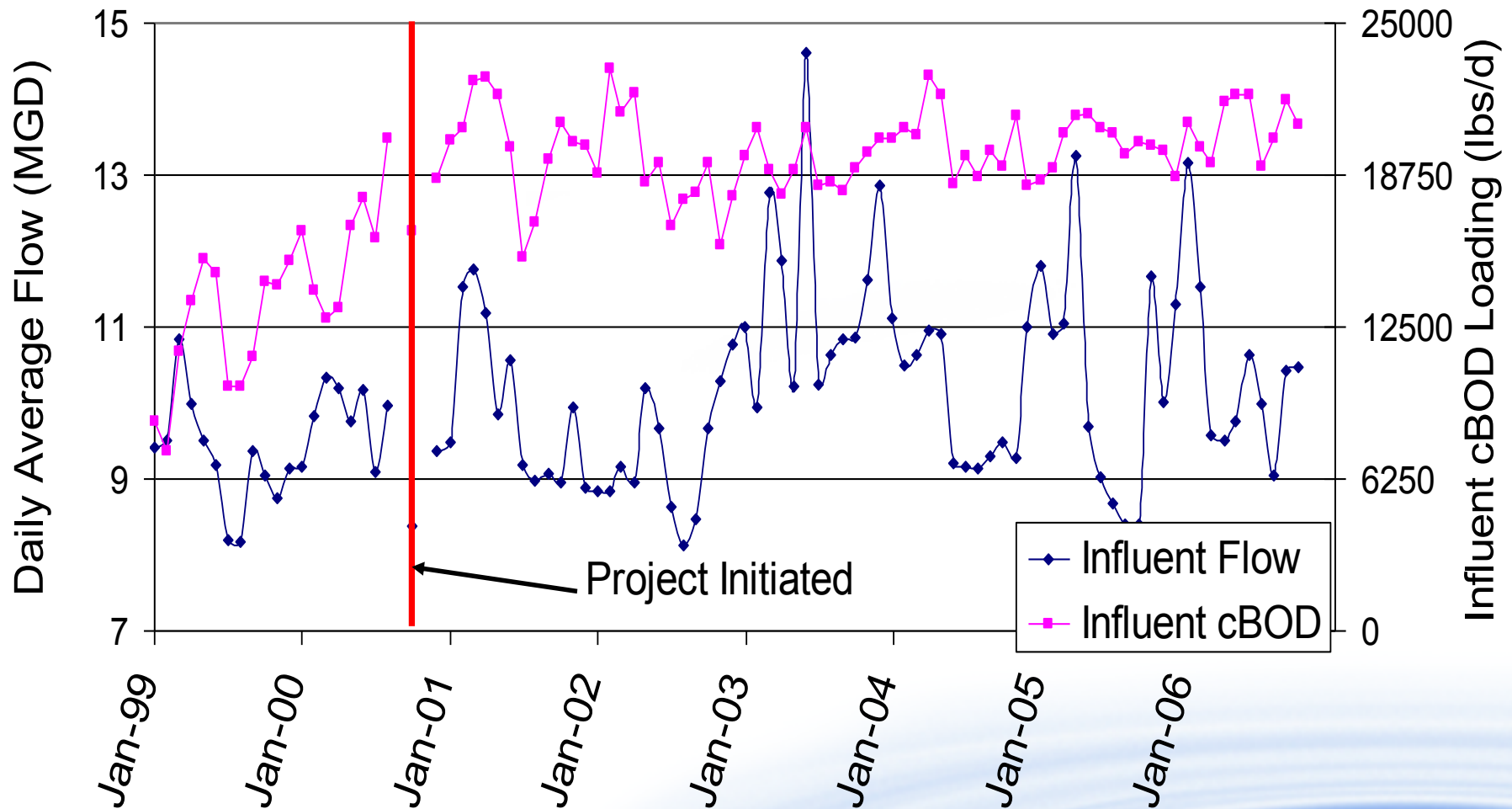
- Stringent permit limits
- Increasing influent flow
- Increasing BOD loading
- High nitrate in Passaic river
- Denitrification occurring in clarifiers

# Issues Facing RVRSA: Increasing Flow and BOD Loading



- Increasing influent flow
  - Flows from ~9 MGD in 1990' s
  - Current daily average flow 11 MGD
- Increasing BOD loading
  - Tighter sanitary sewers
  - Water conservation products

# Issues Facing RVRSA: Increasing BOD Loading





# Issues Facing RVRSA: Nitrate Problems



- High  $\text{NO}_3\text{-N}$  in Passaic River
  - River nitrate concentration approaching or exceeding 10 mg/L drinking water limit
  - Possible reasons
    - Nitrification requirement for all treatment plants upstream of RVRSA
    - Drought conditions

# Issues Facing RVRSA: Denitrification



- Denitrification in the clarifiers
  - “Squirrels”
  - Poor settling due to filaments
  - Periodic incomplete nitrification
    - some  $\text{NH}_3\text{-N}$  violations
  - Difficulty controlling rising blankets
    - had three or four clarifiers online

# Possible Solutions: What RVRSA Could Have Done



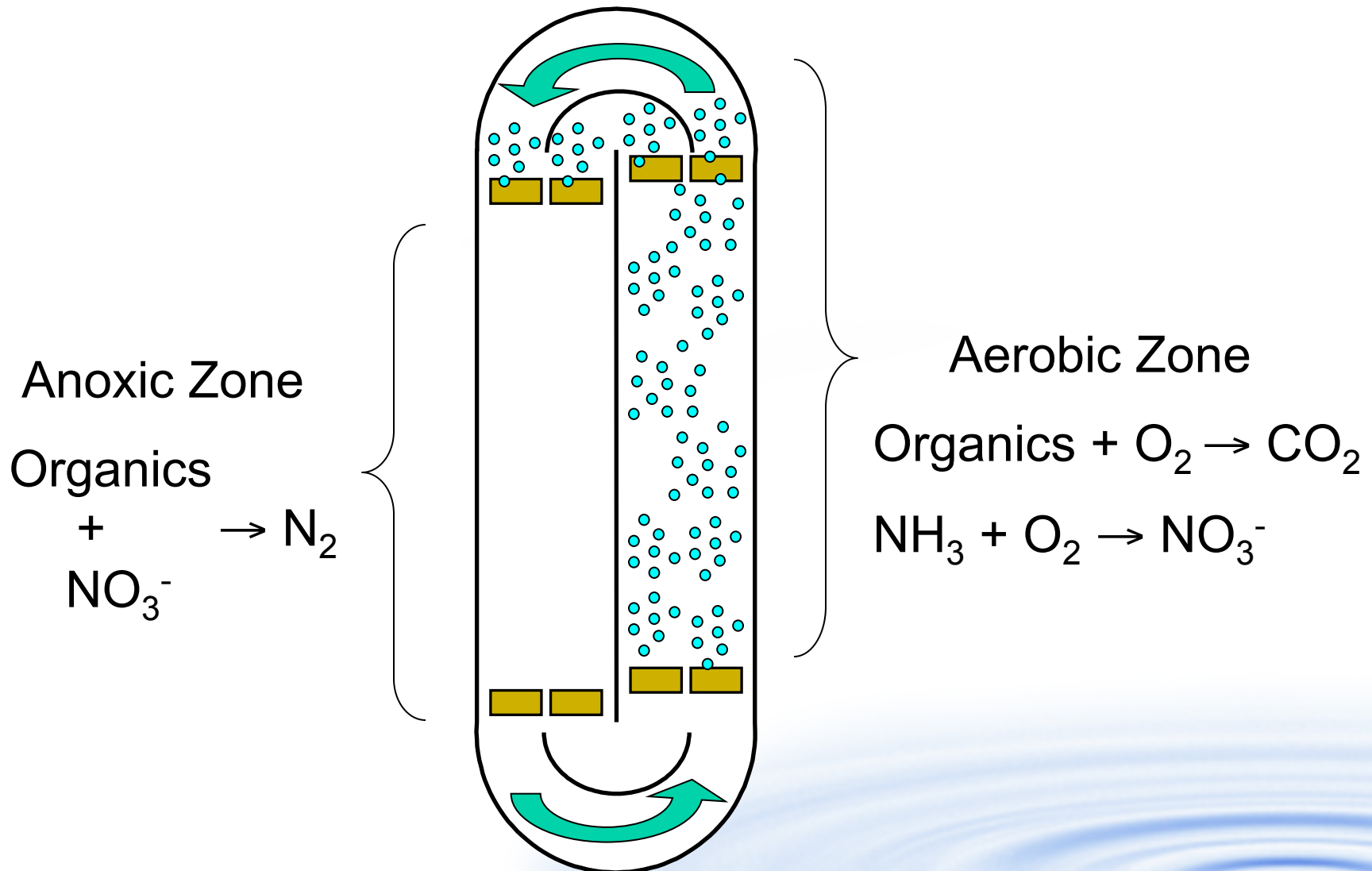
- Use third oxidation ditch for additional cBOD loading
  - Increases aeration hp 50%
- Denitrify with mixed liquor recycle
  - Add anoxic tank
  - Additional pumping costs

# Solution: Tight Operational Process Control



- Process control expert: Bob Sobeck
- Nitrification & denitrification in ditches
  - High DO and low DO zones
  - Turn off some brush aerators
- Take one to two clarifiers offline
- Improved Process Control
  - Better nitrification
  - Increase cBOD loading to ditches
  - More aeration during high  $\text{NH}_3\text{-N}$  loading

# Solution: Denitrification in Oxidation Ditches



# Solution:

## Denitrification in Oxidation Ditches



- Nitrification & Denitrification in Ditches
  - High DO and low DO zones
  - Lower overall average DO
- Methods of Control
  - Ditch effluent ammonia and nitrate several times a day
    - reduce aeration during low  $\text{NH}_3$  loading
  - DO control
  - ORP could be used, other applications

# Solution: Increased Process Control



- Process Control
  - Increase MLSS in the aeration basins to meet increased cBOD loading
  - Allow for better nitrifier growth
  - Requires more aeration time during high  $\text{NH}_3\text{-N}$  loading
- Methods of Control
  - Wasting flow, waste concentration
  - Solids inventory

# Solution: Current vs. Design

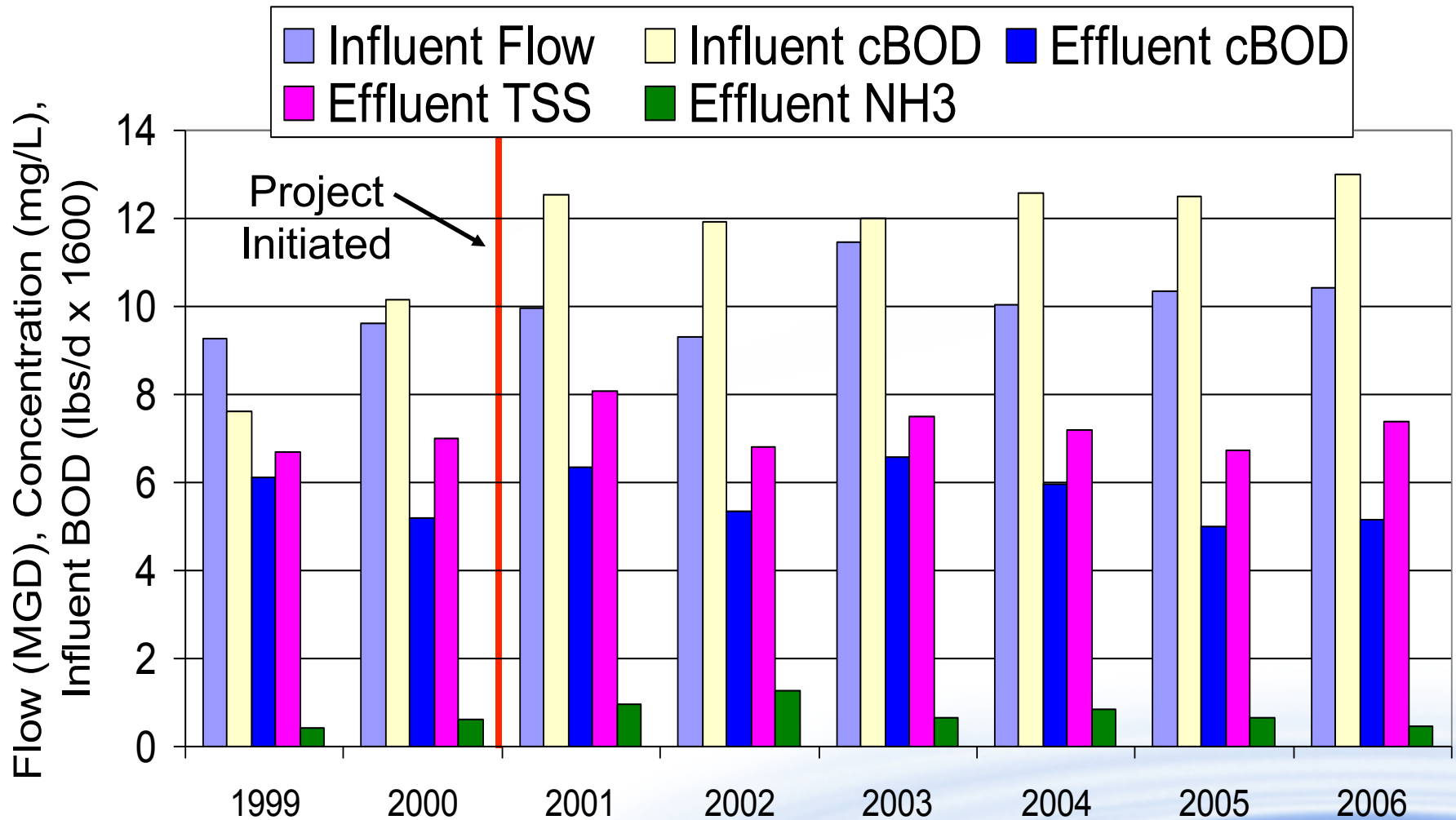


- Comparison of current operational parameters and design parameters

Parameter	Design	Current
HRT, hrs	22.0	12.9
Organic Loading, lbsBOD/1000ft <sup>3</sup> /d	15.1	27.0
Clarifiers, gal/ft <sup>2</sup> /d	382	700
MCRT, days	10+	10
MLSS, mg/L	<2,000	2,400



# Solution: Maintaining Excellent Effluent Quality



# Cost and Energy Savings: Direct Savings



- On/Off Aeration Power Savings
  - 800 hp available (in the two online ditches)
  - Estimated 560 hp used on average
    - More at higher NH<sub>3</sub> loading
    - Less at lower NH<sub>3</sub> loading

$$240 \text{ hp} \times \frac{24 \text{ hr}}{\text{day}} \times \frac{0.746 \text{ kW}}{\text{hp}} \times \frac{\$0.08}{\text{kW} \cdot \text{hr}} = \$344 / d$$

- Savings: \$125,000 / yr

# Cost and Energy Savings: Direct Savings



- Keeping 3<sup>rd</sup> Ditch Offline
  - 200 hp necessary

$$200 \text{ hp} \times \frac{24 \text{ hr}}{\text{day}} \times \frac{0.746 \text{ kW}}{\text{hp}} \times \frac{\$0.08}{\text{kW} \cdot \text{hr}} = \$286 / \text{d}$$

- Savings: \$105,000 / yr
- Total Energy Savings: \$230,000 / yr

# Cost and Energy Savings: Indirect Savings



- Increased oxygen transfer efficiency

$$AOTE = SOTE \cdot \alpha \cdot \frac{(\beta \cdot C_{SW} - C_L)}{9.17 \text{ mg/L}} \cdot \theta^{(T-20)}$$

- At 1000' and 20°C:  $\beta = 0.95$  and  $C_{SW} = 8.9$
- At DO = 2.0 mg/L,  $\frac{(0.95 \times 8.9 - 2.0)}{9.17} = 0.70$
- At DO = 1.0 mg/L,  $\frac{(0.95 \times 8.9 - 1.0)}{9.17} = 0.81$
- Increase in efficiency of 16%

- Reduces chlorine usage
  - Chlorine gas used as disinfectant
  - Less nitrite remaining in effluent to consume chlorine residual
  - Decreased 11%
- Significantly less nitrate to river
  - Not a permit requirement
- Re-rated WWTP
  - Increased the permitted capacity of WWTP from 12.0 MGD to 15.9 MGD

# Other Benefits: Phosphorus Removal



- Presently TP to 1.5 mg/L
- Future Enhanced Biological Nutrient Removal
  - Add anaerobic tank ahead of oxidation ditches
  - TP reliably under 1.0 mg/L w/o chemical
- Future Coagulation and Filtration
  - Add aluminum or iron salt
  - Cloth filters (or sand filters) for TP as low as 0.2 mg/L

# Questions?!